

+ CCUS in Greece: Implementing Hubs for a Low-Carbon Future

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CCUS technology



- Technology that captures CO₂ emissions from industrial processes and either reuses or permanently stores them
- A key solution for reducing greenhouse gas emissions and achieving climate goals
- Greece's industrial emissions and the need for decarbonization
- Alignment with European and global climate targets (e.g. EU Green Deal, net-zero commitments).
- Potential economic and environmental benefits.

CCUS VALUE CHAIN

MAIN COMPONENTS OF CCUS HUB



Study basis: Scope & Approach

Scope

- To analyze the feasibility, costs and challenges of implementing CCUS hub in Attica region.
- To assess different infrastructure components.
- To identify key risks and necessary regulatory frameworks.

Research Foundation

- The study is based on desk research and analysis of relevant bibliographic sources.
- Comparative assessment of European & international projects
- Case studies from similar industrial clusters

Data sources

- Data provided by IENE
- Bibliographic sources
- EU & International Projects
- Vendors consultancy
- Historical data

Legislative & Regulatory Framework

- Study follows European & National CCUS regulations
- Legislative gap: Greek regulations cover CO₂ storage but lack clarity on pipeline transportation
- Framework based on natural gas pipeline regulations and other directives



Cost Estimation

- Cost estimates are based on historical data, vendor input and advanced modeling tools
- Accuracy range: Feasibility study level (-20% to +40% uncertainty).
- Key cost indicators include CAPEX (Capital Expenditure) and OPEX (Operational Expenditure).
- Operational lifecycle considered: 20 years

Key challenges

- Legislative barriers: No clear framework for CO₂ pipeline transport costs in Greece
- Safety & feasibility studies required: Additional costs for high-pressure CO₂ transport & site-specific geological analysis.





CCUS Hub Working Scenarios



The study evaluates different CCUS hub configurations based on CO₂ capture capacity and the number of industrial emitters

Cluster of 3 Industrial Emitters

CCUS Capacity: 5 MTPA

Scenario 1: Industrial Cluster of 3 emitters	5,0
HELPE AIC	1,5
HELPE EIC	1,5
TITAN KAMARI	2,0

Hub indicative location site: Elefsis

• Selected for its accessibility and proximity to existing energy infrastructures

Cluster of 6 Industrial Emitters CCUS Capacity: 5 MTPA

Scenario 2: Industrial Cluster of 6 emitters	5,0
HELPE AIC	1,0
HELPE EIC	1,0
TITAN KAMARI	1,5
HERON II	0,5
PROTERGIA	0,5
ELPEDISON	0,5

CCS Technology



Each industry installs its own CCS (Carbon Capture & Storage) Plant

Indicative technology: First and second generation oxyfuel & Post combustion cryogenic

<u>Process Flow</u>: Capture \rightarrow Pre-treatment (compression & dehydration)

CCS PLANT	1 MTPA
CAPEX ¹	€150-200 million
OPEX ²	€70-75 million

^{1CAPEX} Nominal operational cycle of 45.000kW

^{2 OPEX} Key operational parameters were considered, including a heat demand of 2 GJ per tn of CO_2 , annual O&M costs of 3% of CAPEX, and labor costs ranging from 2-5 million/year.

Carbon Capture System



Cultural & archaeological sites

Pipeline routes must steer clear of site with cultural or archaeological significance.

Safety & population density

Avoid densely populated areas and regions with high ٠ urban or industrial density to minimize risks.

Existing Infrastructure:

Leverage existing roads, railways and energy corridors ٠ (e.g. former natural gas/oil pipelines) to reduce construction and environmental impact.

CO2 Transportation & Positioning Considerations

Proposed design:

- Backbone pipeline complemented by smaller branches ٠ serving individual emitters.
- Allows future expansion and extension of the network.

Key Positioning Elements

Geological and topographical conditions:

- Stable soil conditions and flat or gently undulating terrain Environmental conditions:
- Avoidance of protected areas and environmentally sensitive zones (e.g. aquatic ecosystems that require special permits).





O Asprofos engineering

Geological & Geotectonic Map





Designed

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Checked

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Approved 5 Konstanting Tagings

Size At



Protected & Environmentally Sensitive Areas Map





Niches Dara



Land Uses, Infrastructure & Socioeconomic Environmental Map

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on-tan na Taalapati

Evangelia Gloti

Eithi varryaka

CO₂ transportation Restrictions & Challenges

Connectivity challenge between Aspropyrgos and Elefsis Refineries was encountered.

Available transportation options were explored:

Onshore pipeline may be feasible

• Subject to additional investigation, specific empirical studies & exploration of international standards.

Offshore pipeline is considered infeasible

- High ship density and anchorage
- Shipwreck risk & existing shipwrecks
- Sediment Impact & Marine ecosystem disruption
- Urban Plan Conflicts

Ship

• Not economically efficient.











Project Overview Map

CO₂ pipeline network Cost estimation

CO₂ is transported under supercritical conditions:

- Pressure: 100-110 bar
- Temperature: 20°C

Scenario 1: 32 km of pipeline + connection with AIC & EIC

Scenario 2: 174 km of pipeline

Pipeline network	Scenario I (32 km)	Scenario II (174 km)
CAPEX ¹	€247 million	€388 million
OPEX ²	€ 5 million	€8 million

^{1 CAPEX} includes pipelines and peripheral facilities, civil & mechanical work, project management, detailed design, procurement services and construction supervision. The cost of expropriation is not included.

^{2 OPEX} was estimated with annual O&M costs of 2% of CAPEX.



Material:	Max. Capacity: 5 MTPA		l oneth
Carbon steel	Scenario I	Scenario II	Length
Protergia	0.5		30 km
branch	0,5		JUKIT
Elpedison	0.5		26 km
branch	0,5		ZU KITI
Heron branch	0,5	-	0,5 km
Titan branch	1,5	2	0,5 km
AIC branch	1	1,5	10
EIC branch	1	1,5	1
Main pipeline	5	5	20 km 106 km
Total length			32 km 🛛 174 km

Liquefaction Facility



Comprise:

- Pipeline terminals for receiving emitters' captured CO₂
- Treatment Unit: dehydration & purification, pressure 30-50 bar
- Liquefaction Unit: heat exchangers, cooling towers & refrigeration, pressure 7 bar & temperature -50°C

Liquefaction Facility	5 MTPA
CAPEX	€250-300 million
OPEX ¹	€57-84 million

^{1 OPEX} key operational parameters were considered, including energy cost for liquefaction 90-120 kWh per ton of CO2, a heat cost at \in 115 per MWh, annual maintenance costs of 2-4% of CAPEX annually, and labor costs ranging from 2 to 5 million \in .

Collection terminal



Temporary Storage Facilities



Indicative storage capacity: 55.000 m³

Key assumptions for space estimation

Storage consists of 10 spherical tanks of 5.500 m³

Temporary Storage	55.000 m ³
CAPEX	€93 million
OPEX ¹	€3 million

^{1 CAPEX} includes necessary equipment, piping, instruments, electrical, civil works and painting & insulations works.

^{2 OPEX} was estimated with annual O&M costs of 3% of CAPEX.



Assumptions of transport cycle	
Distance (Elefsis – Prinos Storage Facility)	333,36 km
Ship velocity	22,22 km/hr
Flow rate (loading)	1000 t/hr
Flow rate (unloading)	500 t/hr
Shipment required	15 hr
Loading time	20 hr
Unloading	40 hr
Total transport cycle	90 hr

A vessel would require 3,75 days to complete a full transport. Vessel capacity: 20.000 tn Given liquefaction capacity 5 MTPA Inlet flow: 13.000 tn CO^2/day Storage capacity: 50.000 – 60.000 m³ CO₂ entering at low pressure and temperature, resulting in a higher density and therefore requiring less volume. Member of HELLENIQ ENERGY

Transportation to permanent storage facilities



Indicative number of vessels

To transport 5 MTPA of CO_2 at a permanent storage facility:

- a cycle of three vessels is required
- Capacity per vessel: 20.000 tons

Ship loading facility

- Ship loading pumps
- Three loading arms:
 - Ship loading
 - Vapor return
 - Back-up

Geological Storage Site

Permanently stored via injection into deep geological formations:

• Depleted oil and gas reservoirs

Loading station	Tanker 20.000 tonnes
CAPEX	€20 million
OPEX ¹	€0,6 million

^{1 CAPEX} includes necessary equipment, piping, instruments, electrical, civil works and painting & insulations works.

 $^{\rm 2 \ OPEX}$ was estimated with annual O&M cost set at 3% of CAPEX.

Conclusions & Remarks



- Difficulties in estimating the cost of Carbon Capture System and Liquefaction plant.
- A safety study is required due to the high pressure associated with long distances.
- Areas with steep slopes, such as Thisvi and Aghios Nikolaos, will require additional analysis and study before construction.
- further research and study are necessary for connecting the Aspropyrgos refinery, especially if a legislative framework for such pipelines is introduced.
- CO₂ is non-flammable and non-toxic, it is asphyxiant at high concentrations (displacing oxygen), so a safety study is also required for the temporary storage facility.
- The storage size, along with the frequency and reliability of ship arrivals, should also be assessed.
- Design pressure estimates, based on bibliographic data, need further investigation, particularly for storage and shipping loading, potentially in close cooperation with relevant shipping operators.
- A Front-End Engineering and Design (FEED) study should be conducted for the entire Carbon Capture project, including storage and shipping.
- Constructability also should be assessed.



+ Thank you

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